Amendments to the Claims:

Claims 1-4 (Canceled).

5. (Previously Presented) A process for the preparation of hydrogen and carbon monoxide containing gas from a carbonaceous feedstock said process comprising:
(a) partially oxidizing a carbonaceous feedstock thereby obtaining an effluent comprising a first gaseous mixture of hydrogen and carbon monoxide, and
(b) catalytically steam reforming a carbonaceous feedstock to thereby obtain a steam reformer product, which catalytic steam reforming is carried out in a convective steam reformer comprising a tubular reactor provided with a plurality of parallel positioned steam reformer reactor tubes containing a reforming catalyst, and heat for the steam reforming reaction is provided by convective heat exchange between the steam reformer reactor tubes and one or more passageways positioned within and along the axis of the tubular reactor tubes through which passageway the effluent of step (a) flows counter-current to the gasses in the steam reformer tubes.

6. (Previously Presented) The process of claim 5, wherein the gas velocity in the passageway is between 10 m/s and 60 m/s.

7. (Previously Presented) The process of claim 5, wherein between 0 wt% and 60 wt% of the steam reformer product as obtained in step (b) and the effluent of step (a) flows through the passageway.

8. (Previously Presented) The process of claim 5, wherein the hydrogen to carbon monoxide molar ratio of the combined products of step (a) and (b) is between 1.5 and 3.

9. (Previously Presented) The process of claim 5, wherein the steam to carbon molar ratio of the feed to step (b) is between 0.5 and 0.9.

10. (Previously Presented) The process of claim 9, wherein the reforming catalyst comprises (a) an oxidic support material and (b) a coating comprising between 0.1 wt% and 7.0 wt% of at least one of the metals selected from the group consisting of Pt, Ni, Pd and Co, said support material comprising: (i) at least 80 wt% of ZrO2 which has been calcined at a temperature up to about 670 °C before the application of said coating; and, (ii) 0.5-10 mol% of at least one oxide selected from the group consisting of oxides of Y, La, Al, Ca, Ce and Si.

11. (Previously Presented) The process of claim 5, wherein the passageways of step(b) comprise metal wall surfaces and the temperature of the metal wall surfaces is maintained below 1100 °C.

12. (Previously Presented) The process of claim 5, wherein the steam reforming product of step (b) is fed to step (a).

13. (Previously Presented) The process of claim 12, wherein the steam reforming product of step (b) is fed to the upper half of a partial oxidation reactor vessel having an upper end, said vessel provided with a burner at its upper end, and wherein the temperature in the upper half of the vessel is between 800°C to 1050°C.

14. (Previously Presented) The process of claim 12, further comprising:

(c) autothermally reforming a mixture of the steam reformer product of step (b) and the product of the partial oxidation reaction of step (a).

15. (Previously Presented) The process of claim 5, wherein hydrogen is recovered from the effluent of step (b).

16. (Previously Presented) The process of claim 5, wherein step (b) is performed in a reactor vessel for performing a steam reforming reaction comprising:
a vessel inlet for natural gas and steam,
a vessel inlet for a hot gaseous medium,

a vessel outlet for a gaseous product comprising the steam reforming product; and

a reactor space having a reactor space inlet and a reactor space outlet end, the reactor space comprising a bed of steam reforming catalyst, the reactor space inlet being fluidly connected to the inlet for natural gas and steam, and at the reactor space outlet end being fluidly connected with the outlet for the gaseous product;

wherein inside the catalyst bed a passageway fluidly connects to the vessel inlet for the hot gaseous medium, the passageway being suitable for passage of hot gaseous mixture counter currently to a flow of reactants in the catalyst bed.